

# 淡江大學九十一年度碩士班招生考試試題

系列：化學工程學系

科目：化工熱力學 50%

86-1

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### Problem 1: 20 points

One kmole of ideal gas with a heat capacity of  $C_p = 29.3 \text{ kJ/kmol}\cdot\text{K}$  undergoes the following three-step process:

Step 1: The gas is heated at constant volume from 300K and 0.1 MPa until the pressure reaches 0.2 MPa.

Step 2: The gas is expanded adiabatically and reversibly to a pressure of 0.1 MPa.

Step 3: At a constant pressure of 0.1 MPa, the gas is cooled to 300K.

**Determine the heat and work effects for each step.**

(Gas constant  $R = 8.314 \text{ kJ/kmol}\cdot\text{K} = 0.008314 \text{ MPa}\cdot\text{m}^3/\text{kmol}\cdot\text{K}$ )

### Problem 2: 10 points

Calculate the **fugacity** of carbon dioxide at 100°F and 200 psia using the generalized property diagram as shown in Figure 1. The critical pressure and critical temperature of carbon dioxide are 72.9 atm and 304.2K, respectively.

### Problem 3: 20 points

Assume benzene and toluene form an ideal solution, which follows the Raoult's Law. Calculate the phase equilibrium **vapor composition** and **liquid composition** for a benzene and toluene mixture at 90°C and 1 atm.

The Antoine equation is:

$$\log P^\circ = A - \frac{B}{C+t}, \text{ where } P^\circ \text{ in mmHg and } t \text{ in } ^\circ\text{C}.$$

The parameters for Antoine equation are:

|         | A       | B        | C       |
|---------|---------|----------|---------|
| benzene | 6.90565 | 1211.033 | 220.790 |
| toluene | 6.95334 | 1343.943 | 219.377 |

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系別：化學工程學系

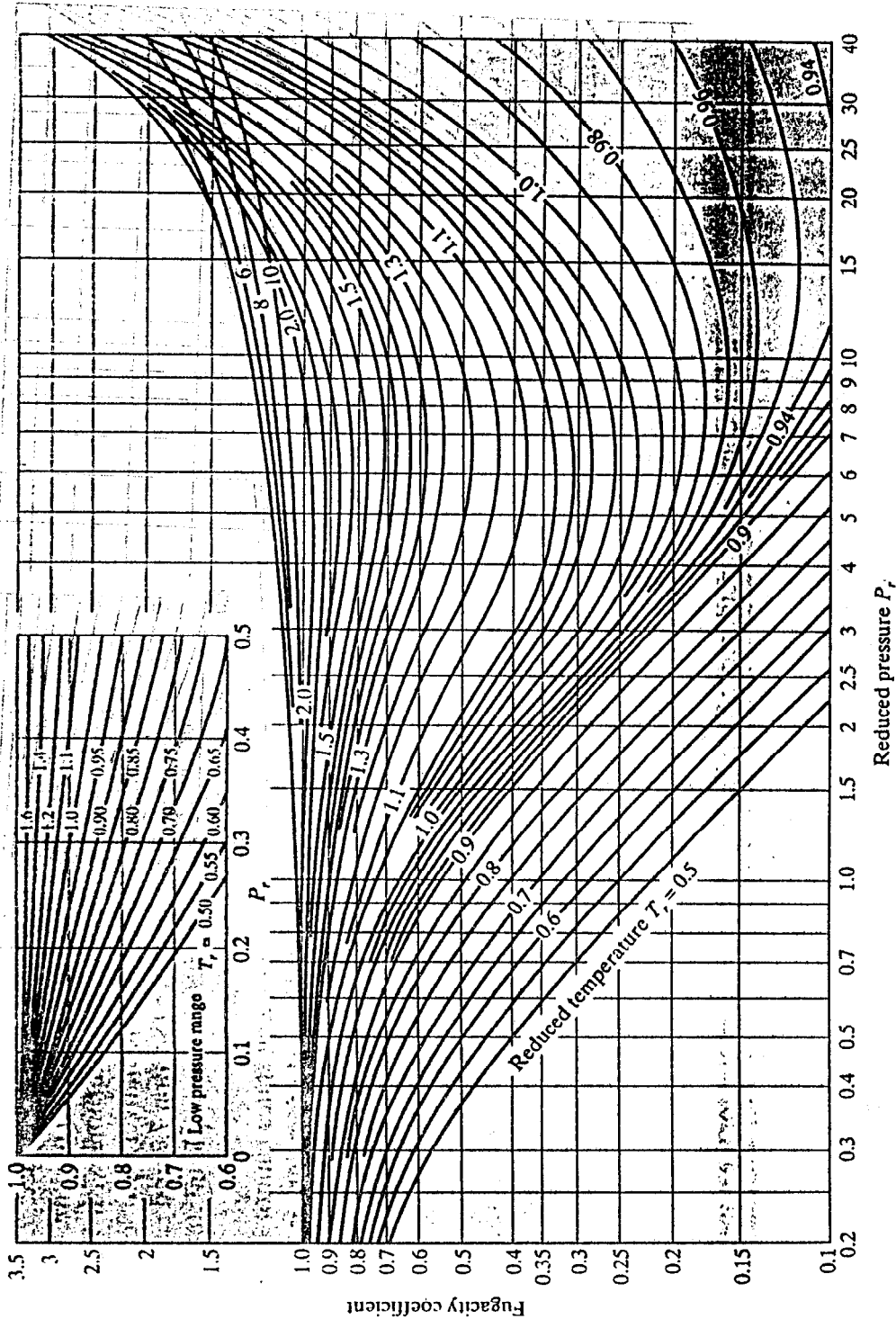
科目：化工熱力學 50%

96-2

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Figure 1



# 淡江大學九十一學年度碩士班招生考試試題

86-3

系別：化學工程學系

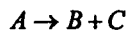
科目：化學反應工程 50%

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1. How many types of industrial reactors do you remember? When are the reactors used? Describe the advantages and disadvantages of these reactors in detail. (20%)

2. A liquid-phase elementary reaction



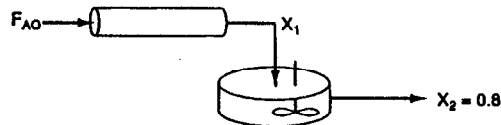
is irreversible and the rate law is

$$-r_A = kC_A$$

where the rate constant  $k$  is  $0.01 \text{ s}^{-1}$ .

Calculate the individual reactor volume and the total reactor volume for each scheme shown in the attached figure. The intermediate conversion,  $X_1$ , is 0.4, the final conversion,  $X_2$ , is 0.8, the entering volumetric flow rate,  $v_0$ , is  $1 \text{ dm}^3/\text{s}$ , and the entering molar flow rate of A,  $F_{A0}$ , is  $0.5 \text{ mol/s}$ . (30%)

Scheme A



Scheme B

