# 淡江大學 97 學年度碩士班招生考試試題

系別:化學工程與材料工程學系 科目:化學反應工程

准带項目請打「V」

✓ 簡單型計算機

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### Problem 1

Consider the elementary liquid-phase reaction,  $A+B\to P$ , with reaction rate constant k=1 m<sup>3</sup>/(kmole-s). Suppose inlet concentration of feed,  $C_{A,in}=C_{B,in}=10$  kmloe/m<sup>3</sup>. It is desired to achieve an output concentration  $C_{A,out}=1$  kmloe/m<sup>3</sup>.

(a) Find the mean residence time needed to achieve this value using a PFR. (15pt)

(b) Repeat (a) assuming that the reaction occurs in a CSTR. (15pt)

## Problem 2 (30pt)

A liquid-phase reaction,  $A + water \rightarrow C$ , is carried out in a well-mixed batch reactor. In the reactor, 500 ml of a 2 M solution (2 kmloe/m³) of A in water is mixed with 500 ml of water. The temperature was maintained at 50 °C. The concentration of product C,  $C_C$ , is recorded as a function of time as follows:

| Time  | Cc         |  |  |  |  |
|-------|------------|--|--|--|--|
| (min) | (kmloe/m³) |  |  |  |  |
| 0     | 0          |  |  |  |  |
| 0.5   | 0.145      |  |  |  |  |
| 1.0   | 0.270      |  |  |  |  |
| 1.5   | 0.376      |  |  |  |  |

Using the data shown above, determine the rate constant k at 50 °C. The water concentration can be assumed to be constant, and the reaction is first-order in component A.

Hint: Natural logarithms of numbers

| n 1.0 1.1 1.2 1.3 1.4 1.5 1.6 1.7 1.8                                |       |                                   |        |        |        |        |     |       |
|----------------------------------------------------------------------|-------|-----------------------------------|--------|--------|--------|--------|-----|-------|
|                                                                      | n     | 1.5 1.6 1.7 1.8 1.9               | 1.4    | 1.3    | 1.2    | 1.1    | 1.0 | n     |
| ln(n) 0.0 0.0953 0.1823 0.2624 0.3365 0.4055 0.4700 0.5306 0.5878 0. | ln(n) | .4055 0.4700 0.5306 0.5878 0.6419 | 0.3365 | 0.2624 | 0.1823 | 0.0953 | 0.0 | ln(n) |

#### Problem 3

The irreversible first-order gas-phase reaction,  $A \to C$ , is carried out isothermally in a fluidized-catalytic CSTR containing 50 kg of catalyst. There is no pressure drop in the CSTR, and a 50% conversion is obtained for pure A entering at pressure of 20 atm.

- (a) The same reaction is carried out isothermally in a packed-bed catalytic reactor (PBR) containing 50 kg of catalyst, and pure A enters the PBR at pressure of 20 atm. Assuming there is no pressure drop along the packed-bed, what is the conversion exiting the PBR? (20pt)
- (b) Repeat (a) assuming the pressure drop along the PBR follows  $P = P_{in}(1 0.02W)^{1/2}$ , where  $P_{in}$  is the inlet pressure and W is the catalyst weight in kg. (10pt)

Hint:  $\exp(2/3) = 1.948$ ,  $\exp(1) = 2.718$ ,  $\exp(3/2) = 4.482$ 

## Problem 4 (10pt)

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